

Answers to problems

2. Characteristics of fluids

1. kg m/s^2
2. Viscosity: Pa s, Kinematic viscosity: m^2/s
3. $v = 0.001 \text{ m}^3/\text{kg}$
4. $2.06 \times 10^7 \text{ Pa}$
5. $h = \frac{2T \cos \theta}{\rho g b}$, $h = 1.48 \text{ cm}$
6. 291 Pa
7. $9.15 \times 10^{-3} \text{ N}$
8. 1.38 N
9. 1461 m/s

3. Fluid statics

1. $6.57 \times 10^7 \text{ Pa}$
2. (a) $p = p_0 + \rho g H$,
(b) $p = p_0 - \rho g H$,
(c) $p = p_0 + \rho' g H' - \rho g H$
3. (a) $p_1 - p_2 = (\rho' - \rho) g H + \rho g H_1$,
(b) $p_1 - p_2 = (\rho - \rho') g H$
4. 50 mm
5. Total pressure $P = 9.56 \times 10^5 \text{ N}$, $h_c = 6.62 \text{ m}$

6. $2.94 \times 10^4 \text{ N}$, 5.87×10^4
7. $9.84 \times 10^3 \text{ N}$
8. Force acting on the unit width: $1.28 \times 10^6 \text{ N}$, Action point located along the wall from the water surface: 11.6 m
9. 7700 N m
10. Horizontal component $P_x = 1.65 \times 10^5 \text{ N}$, Vertical component $P_y = 1.35 \times 10^5 \text{ N}$, total pressure $P = 2.13 \times 10^5 \text{ N}$, acting in the direction of 39.3° from a horizontal line
11. 976 m^3
12. $h = 0.22 \text{ m}$, $T = 0.55 \text{ s}$
13. $\omega = \frac{1}{r_0} \sqrt{2gh}$ rad/s, $\omega = 14 \text{ rad/s}$ at $h = 10 \text{ cm}$, speed of rotation when the cylinder bottom begins to appear $n = 4.23 \text{ s}^{-1} = 254 \text{ rpm}$

4. Fundamentals of flow

1. (a) A flow which does not change as time elapses is called a **steady** flow. **Velocity**, **pressure** and **density** of flow in a steady flow are functions of position only, and most of the flows studied in hydrodynamics are steady flows. A flow which changes as time elapses is called an **unsteady** flow. **Velocity**, **pressure** and **density** of flow in an unsteady flow are functions of **time** and **position**. Flows such as when a valve is **opened** / **closed** or the **discharge** from a tank belong to this flow.
 - (b) The flow velocity is **proportional** to the radius for a free vortex flow, and is **inversely** **proportional** to the radius for a forced vortex flow.
2. $\Gamma = 0.493 \text{ m}^2/\text{s}$
3. $Re = 6 \times 10^4$, turbulent flow
4. $\frac{dx}{x} = -\frac{dy}{y}$ namely $xy = \text{const}$
5. (a) Rotational flow
 (b) Irrotational flow
 (c) Irrotational flow

6. Water $v_c = 23.3 \text{ cm/s}$, air $v_c = 3.5 \text{ m/s}$
 7. $\Gamma = 82 \text{ m}^2/\text{s}$

5. One-dimensional flow

1. See text.
 2. $v_1 = 6.79 \text{ m/s}$, $v_2 = 4.02 \text{ m/s}$, $v_3 = 1.70 \text{ m/s}$
 3. $p_2 = 39.5 \text{ kPa}$, $p_3 = 46.1 \text{ kPa}$
 4. p_0 : Atmospheric pressure, p : Pressure at the point of arbitrary radius r

$$p_0 - p = \frac{\rho Q^2}{8\pi^2 h^2} \left(\frac{1}{r^2} - \frac{1}{r_2^2} \right)$$

$$\text{Total pressure (upward direction) } P = \frac{\rho Q^2}{4\pi h^2} \left[\log \frac{r_2}{r_1} - \frac{1}{2} \left(1 - \frac{r_1^2}{r_2^2} \right) \right]$$

5. $v_r = 5.75 \text{ m/s}$, $p_r - p_0 = -1.38 \times 10^4 \text{ Pa}$
 6. $t = \frac{2A\sqrt{H}}{Ca\sqrt{2g}}$
 7. Condition of section shape $H = \left(\frac{\pi v}{Ca\sqrt{2g}} \right)^2 r^4$
 $Q = 12.9 \text{ m}^3/\text{s}$, $d = 1.29 \text{ mm}$
 8. $H = 2.53 \text{ m}$
 9. $Q_1 = \frac{1 + \cos \theta}{2} Q$, $Q_2 = \frac{1 - \cos \theta}{2} Q$, $F = \rho Q v \sin \theta$
 $Q_1 = 0.09 \text{ m}^3/\text{s}$, $Q_2 = 0.03 \text{ m}^3/\text{s}$, $F = 2.53 \times 10^4 \text{ N}$
 10. $-7.49 \text{ mH}_2\text{O}$
 11. $n = 6.89 \text{ s}^{-1} = 413 \text{ rpm}$, torque $8.50 \times 10^{-2} \text{ N m}$
 12. $F = 749 \text{ N}$

6. Flow of viscous fluids

1. See text.
 2. $\frac{1}{r} \frac{\partial(rv)}{\partial r} + \frac{\partial u}{\partial x} = 0$, or $\frac{\partial v}{\partial r} + \frac{v}{r} + \frac{\partial u}{\partial x} = 0$
 3. (a) $u = 6v \left[\frac{y}{h} - \left(\frac{y}{h} \right)^2 \right]$,
 (b) $v = \frac{1}{1.5} u_{\text{max}}$

$$(c) Q = \frac{h^3}{12\mu} \frac{\Delta p}{l},$$

$$(d) \Delta p = \frac{12\mu l Q}{h^3}$$

$$4. (a) u = 2v \left[1 - \left(\frac{r}{r_0} \right)^2 \right]$$

$$(b) v = \frac{1}{2} u_{\max}$$

$$(c) Q = \frac{\pi d^4}{128\mu} \frac{\Delta p}{l}$$

$$(d) \Delta p = \frac{128\mu l Q}{\pi d^4}$$

$$5. (a) v = 0.82u_{\max},$$

$$(b) r = 0.76r_0$$

$$6. \varepsilon = 4.57 \times 10^{-5} \text{ m}^2/\text{s}, l = 2.01 \text{ cm}$$

$$7. Q = \frac{\pi d h^3}{12\mu} \frac{\Delta p}{l}$$

$$8. h_2 = 0.72 \text{ mm}$$

$$9. \text{LT}^{-1}$$

$$10. 8.16 \text{ N}$$

7. Flow in pipes

1, 2, 3, 4. See applicable texts.

5. See applicable text. Error of loss head h is 5α (%)

6. $h = 733 \text{ m}$ at diameter 50 mm , $h = 26.4 \text{ m}$ at diameter 100 mm

7. 24.6 kW

8. Pressure loss $\Delta p = 508 \text{ Pa}$

9. $3.2 \text{ cm H}_2\text{O}$

10. $h_s = 6.82 \text{ cm}$, $\eta = 0.91$

8. Flow in water channel

$$1. i = \frac{4.56}{1000}$$

2. From Chézy's equation $Q = 40.4 \text{ m}^3/\text{s}$, from Manning's equation $Q = 40.9 \text{ m}^3/\text{s}$
3. $Q = 19.3 \text{ m}^3/\text{s}$
4. Flow velocity becomes maximum at $\theta = 257.5^\circ$, $h = 2.44 \text{ m}$ and discharge becomes maximum at $\theta = 308^\circ$, $h = 2.85 \text{ m}$
5. Tranquil flow, $E = 1.52 \text{ m}$
6. $h_c = 0.972 \text{ m}$, 3.09 m/s
7. $Q_{\max} = 14.4 \text{ m}^3/\text{s}$
8. 1.18 m
9. See applicable text.

9. Drag and lift

1. Using Stokes equation, terminal velocity $v = \frac{d^2 g}{18\nu} \left(\frac{\rho_s}{\rho_w} - 1 \right)$ where d is diameter of a spherical sand particle and ρ_w, ρ_s are density of water and sand respectively.
2. $D = 1450 \text{ N}$, Maximum bending moment $M_{\max} = 3620 \text{ N m}$
3. $D = 2.70 \text{ N}$
4. $\delta_{\max} = 3.2 \text{ cm}$ at wind velocity 4 km/h , $\delta_{\max} = 4.1 \text{ cm}$ at wind velocity 120 km/h
5. $T = 722 \text{ N m}$, $L = 4.54 \times 10^4 \text{ N m/s}$
- 6, 7. See texts.
8. $D_f = 88.9 \text{ N}$, Required power $P = 133 \text{ N m/s}$
9. $L = 3.57 \text{ N}$
10. $D = 134 \text{ N}$

10. Dimensional analysis and law of similarity

1. Consider v, g, H as the physical influencing quantities and perform dimensional analysis. $v = C\sqrt{gH}$
2. $D = C\mu U d$
3. $a = C\sqrt{\frac{K}{\rho}}$
4. $D = \rho L^2 v^2 f\left(\frac{v}{\sqrt{Lg}}\right)$

5. $Q = C \frac{d^4 \Delta p}{\mu l}$

6. $\delta = x f\left(\frac{Ux}{\nu}\right)$

7. $C = f\left(\frac{d\sqrt{2\rho\Delta p}}{\mu}\right) = f(Re)$

8. (a) 167 m/s

(b) 33.3 m/s

(c) 11.1 m/s

9. Towing velocity for the model $v_m = 2.88$ m/s

10. $\frac{1}{2.36}$

11. Measurement of flow velocity and flow rate

1. $v = 4.44$ m/s

2. $v = 28.5$ m/s

3. Mass flow rate $m = 0.325$ kg/s

4. $C_c = 0.64$, $C_v = 0.95$, $C = 0.61$

5, 6, 7. See applicable texts.

8. $U = 50$ cm/s

9. See applicable texts.

10. Error for rectangular weir is 3%, error for triangular is 5%.

12. Flow of ideal fluid

1. $\phi = u_0x + v_0y$, $\psi = u_0y - v_0x$

2. See applicable text.

3. Flow in counterclockwise rotary motion, $v_\theta = \Gamma/2\pi r$, $v_r = 0$, around the origin.

4. $\phi = \frac{q}{2\pi} \log r$, $\psi = \frac{q}{2\pi} \theta$

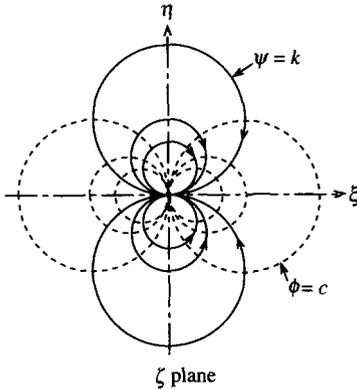
5. Putting $r = r_0$, $\psi = 0$, the circumference becomes one stream line. Velocity distribution $v_\theta = -2U \sin \theta$, Pressure distribution $\frac{p - p_\infty}{\rho U^2/2} = 1 - 4 \sin^2 \theta$

6. The flow around a rectangular corner.

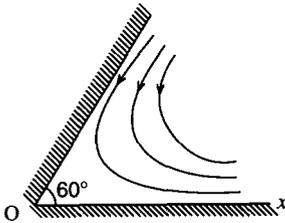
7. Flow in clockwise rotary motion, $v_\theta = -\frac{\Gamma}{2\pi r}$, $v_r = 0$, around the origin.

8. $w = Uze^{-ia}$

9.



10.



13. Flow of a compressible fluid

1. $\rho = \frac{p}{RT} = 1.226 \text{ kg/m}^3$

2. $a = \sqrt{kRT} = 1297 \text{ m/s}$

3. $T_2 = T_1 + \frac{1}{2} \frac{\kappa - 1}{\kappa} R (u_1^2 - u_2^2) = 418 \text{ K}$

$t_2 = 145^\circ\text{C}$

$p_2 = p_1 \left(\frac{T_1}{T_2} \right)^{\kappa/(\kappa-1)} = 3.4 \times 10^5 \text{ Pa}$

4. $T_0 = 278.2 \text{ K}$, $t_0 = 5.1^\circ\text{C}$

$p_0 = 6.81 \times 10^4 \text{ Pa}$

$\rho_0 = 0.85 \text{ kg/m}^3$

5. $v = 444 \text{ m/s}$

6. $M = 0.73$, $a = \sqrt{\kappa RT} = 325 \text{ m/s}$, $v = aM = 237 \text{ m/s}$

7. $v = 272 \text{ m/s}$
8. $\frac{p}{p_0} = 0.45 < 0.528$, $m = 0.0154 \text{ kg/s}$
9. $\frac{A_2}{A_*} = 1.66$
10. $A_2 = 2354 \text{ cm}^2$
11. $2.35 \times 10^5 \text{ N}$
12. Mach number 0.58, flow velocity 246 m/s, pressure $2.25 \times 10^5 \text{ Pa}$

14. Unsteady flow

1. $\frac{dz}{dt} = \pm 1.39 \text{ m/s}$, $T = 1.57 \text{ s}$
2. $T = 2\pi \sqrt{\frac{l}{g(\sin \theta_1 + \sin \theta_2)}}$
3. 0.69 m/s
4. $t = 1 \text{ min } 20 \text{ s}$
5. $a = 837 \text{ m/s}$
6. $\Delta p = 2.51 \times 10^6 \text{ Pa}$
7. $p_{\max} = 1.56 \times 10^6 \text{ Pa}$